

PRIMER PARCIAL

$$\frac{dm_{cv}}{dt} + \Delta(\rho u A)_{fs} = 0 \quad \text{Ecuación de continuidad}$$

Ecuación de Virial

$$z = 1 + \frac{B}{V} + \frac{C}{V^2} + \frac{D}{V^3} + \dots \quad z = 1 + B'P + C'P^2 + D'P^3$$

Correlación de Pitzer

$$z = z^0 + \omega z^1$$

Correlación para el segundo coeficiente de virial

$$z^0 = 1 + B^0 \frac{P_r}{T_r} \quad B^0 = 0,083 - \frac{0,422}{T_r^{1,6}}$$
$$z^1 = B^1 \frac{P_r}{T_r} \quad B^1 = 0,139 - \frac{0,172}{T_r^{4,2}}$$

Ecuación de estado cúbica genérica

$$P = \frac{RT}{V-b} - \frac{a(T)}{(V+\epsilon b)(V+\sigma b)}$$

$$a(T) = \psi \frac{\alpha(T_r) R^2 T_c^2}{P_c} \quad b = \Omega \frac{RT_c}{P_c}$$

Vapor y las raíces de la ecuación de estado cúbica genérica

$$V = \frac{RT}{P} + b - \frac{a(T)(V-b)}{P(V+\epsilon b)(V+\sigma b)}$$

$$z = 1 + \beta - q\beta \frac{(Z-\beta)}{(Z+\epsilon\beta)(Z+\sigma\beta)}$$

$$\beta = \Omega \frac{P_r}{T_r} \quad q = \psi \frac{\alpha(T_r)}{\Omega T_r}$$

Líquido y las raíces de la ecuación de estado cúbica genérica

$$V = b + (V+\epsilon b)(V+\sigma b) \left[\frac{RT + bP - VP}{a(T)} \right]$$

$$z = \beta + (Z+\epsilon\beta)(Z+\sigma\beta) \left(\frac{1+\beta-Z}{q\beta} \right)$$

Parámetros de la ecuación de estado

Ecuación	$\alpha(T_r)$	σ	ε	Ω	ψ	Z_c
vdW	1	0	0	1/8	27/64	3/8
RK	$T_r^{-1/2}$	1	0	0,08664	0,42748	1/3
SRK	$\alpha_{SRK}(T_r; \omega)$	1	0	0,08664	0,42748	1/3
PR	$\alpha_{PR}(T_r; \omega)$	$1 + \sqrt{2}$	$1 - \sqrt{2}$	0,07780	0,45724	0,30740

$$\alpha_{SRK}(T_r, \omega) = \left[1 + (0,480 + 1,574\omega - 0,176\omega^2)(1 - T_r^{1/2}) \right]^2$$

$$\alpha_{PR}(T_r, \omega) = \left[1 + (0,37464 + 1,5422\omega - 0,26992\omega^2)(1 - T_r^{1/2}) \right]^2$$

Ecuación de Racket

$$V^{sat} = V_c Z_c^{(1-T_r)^{0,2857}}$$

Proceso adiabático reversible para gases ideales (Cp=cte)

$$PV^\gamma = cte$$

$$W = \frac{RT_1}{\gamma - 1} \left[\left(\frac{P_2}{P_1} \right)^{(\gamma-1)/\gamma} - 1 \right]$$

Proceso politrópico para gases ideales (Cp=cte)

$$PV^\delta = cte$$

$$W = \frac{RT_1}{\delta - 1} \left[\left(\frac{P_2}{P_1} \right)^{(\delta-1)/\delta} - 1 \right]$$

$$Q = \frac{(\delta - \gamma)RT_1}{(\delta - 1)(\gamma - 1)} \left[\left(\frac{P_2}{P_1} \right)^{(\delta-1)/\delta} - 1 \right]$$

Coefficiente de expansión volumétrica

$$\beta = \frac{1}{V} \left(\frac{\partial V}{\partial T} \right)_P$$

Compresibilidad isotérmica

$$\kappa = -\frac{1}{V} \left(\frac{\partial V}{\partial P} \right)_T$$

Propiedades fundamentales

$$dU = TdS - PdV$$

$$dA = -PdV - SdT$$

$$dH = TdS + VdP$$

$$dG = VdP - SdT$$

Ecuaciones de Maxwell

$$\left(\frac{\partial T}{\partial V}\right)_S = -\left(\frac{\partial P}{\partial S}\right)_V \quad \left(\frac{\partial T}{\partial P}\right)_S = \left(\frac{\partial V}{\partial S}\right)_P \quad \left(\frac{\partial P}{\partial T}\right)_V = \left(\frac{\partial S}{\partial V}\right)_T \quad \left(\frac{\partial V}{\partial T}\right)_P = -\left(\frac{\partial S}{\partial P}\right)_T$$

Prop. Para líquidos

$$dH = C_p dT + (1 - \beta T)VdP \quad dS = \frac{C_p}{T} dT - \beta VdP$$

Prop. Residuales

$$\frac{G^R}{RT} = \int_0^P (Z - 1) \frac{dP}{P} \quad (T = cte)$$

$$d\left(\frac{G^R}{RT}\right) = \frac{V^R}{RT} dP - \frac{H^R}{RT^2} dT$$

Ecuación de Clapeyron

$$\frac{dP^{sat}}{dT} = \frac{\Delta H^{\alpha\beta}}{T\Delta V^{\alpha\beta}}$$

Ecuación Clausius – Clapeyron

$$\frac{d \ln P^{sat}}{d(1/T)} = -\frac{\Delta H^{\alpha\beta}}{R}$$

SEGUNDO PARCIAL

Ecuación de Antoine

$$\ln P_i^{sat} = A - \frac{B}{C + T}$$

Iteración con Ley de Rault

$$T = x_i T_i^{sat} + (1 - x_i) T_i^{sat}$$

$$\alpha = \exp[A_1 - A_2 - \frac{B_1}{C_1 + T} + \frac{B_2}{C_2 + T}]$$

$$P_2^{sat} = \frac{P}{x_1 \alpha + x_2}$$

$$P_i^{sat} = P(y_i + y_2 \alpha)$$

Balance de masa

$$z_i = x_i L + y_i V$$

$$\frac{G^E}{RT} = \sum x_i \ln \gamma_i \quad \sum x_i d \ln \gamma_i = 0$$

Modelos para la energía de Gibbs de exceso

$$\frac{G^E}{x_1 x_2 RT} = A \quad \ln \gamma_1 = A x_2^2 \quad \ln \gamma_2 = A x_1^2$$

Margules

$$\frac{G^E}{x_1 x_2 RT} = A_{21} x_1 + A_{12} x_2 \quad \ln \gamma_1 = x_2^2 [A_{12} + 2(A_{21} - A_{12}) x_1] \quad \ln \gamma_2 = x_1^2 [A_{21} + 2(A_{12} - A_{21}) x_2]$$

Coeficiente de Fugacidad

$$\ln \phi_1 = \int_0^P (Z - 1) \frac{dP}{P}$$

$$\phi_1 = \exp \left[\frac{P_r}{T_r} (B^0 + \omega B^1) \right] \quad B^0 = 0,083 - \frac{0,422}{T_r^{1,6}} \quad B^1 = 0,139 - \frac{0,172}{T_r^{4,2}}$$

$$\ln \hat{\phi}_1 = \frac{P}{RT} (B_{11} + y_2^2 \delta_{12}) \quad \ln \hat{\phi}_2 = \frac{P}{RT} (B_{22} + y_1^2 \delta_{12})$$

$$\delta_{12} = 2B_{12} - B_{11} - B_{22}$$

Fugacidad de un líquido puro

$$f_i = \phi_i^{\text{sat}} P_i^{\text{sat}} \exp \left[\frac{V_i^{\text{sat}} (P - P_i^{\text{sat}})}{RT} \right]$$

$$d(nG) = (nV)dP - (nS)dT + \sum \mu_i dn_i$$

Ecuación de Gibbs/Duhem:

$$\left(\frac{\partial M}{\partial P} \right)_{T,x} dP + \left(\frac{\partial M}{\partial T} \right)_{P,x} dT - \sum_i x_i d\bar{M}_i = 0$$

$$\bar{M}_1 = M + x_2 \frac{\partial M}{\partial x_1} \quad \bar{M}_2 = M - x_1 \frac{\partial M}{\partial x_1}$$

Entalpía, Entropía y Energía Libre de Gibbs

$$H^{id} = \sum y_i H_i \quad S^{id} = \sum y_i S_i - R \sum y_i \ln y_i$$

$$G^{id} = \sum y_i G_i + RT \sum y_i \ln y_i$$

Propiedades fundamentales

$$d \left(\frac{nG}{RT} \right) = \frac{1}{RT} nV dP - \frac{nH}{RT^2} dT + \sum_i \frac{\bar{G}_i}{RT} dn_i$$

$$d \left(\frac{nG^R}{RT} \right) = \frac{nV^R}{RT} dP - \frac{nH^R}{RT^2} dT + \sum_i \frac{\bar{G}_i^R}{RT} dn_i \quad d \left(\frac{nG^E}{RT} \right) = \frac{nV^E}{RT} dP - \frac{nH^E}{RT^2} dT + \sum_i \frac{\bar{G}_i^E}{RT} dn_i$$